

Lecture 13 – Conservation of mass

Purdue ME 200, Thermodynamics I

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Outline

Background and notation

Calculating mass flows

Conservation of mass

Example

Open and closed systems

- a **closed system** or **control mass** is a fixed quantity of matter
- an **open system** or **control volume** is a region of space
- the boundary of a control volume is called a **control surface**

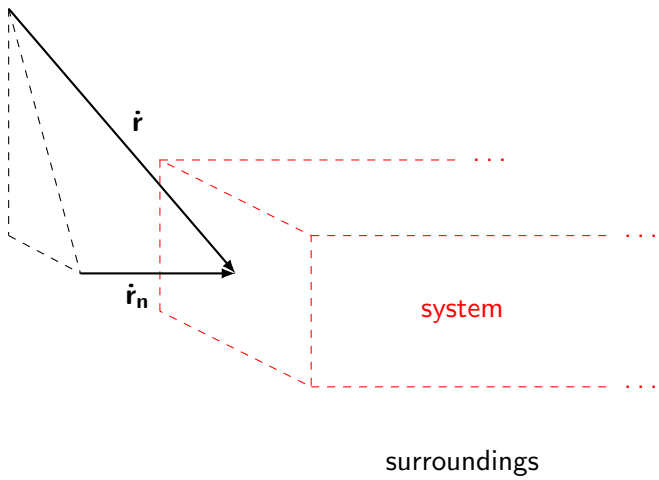
	open	closed
energy crosses boundary?	yes	yes
matter crosses boundary?	yes	no

Velocity and volume notation

- Moran et al. use V for velocity in this chapter
- but we already use V for volume and v for specific volume
- so we'll call velocity $\dot{\mathbf{r}}$
- this follows mechanics notation:
 - ◇ position vector is \mathbf{r}
 - ◇ velocity vector is $\dot{\mathbf{r}}$
 - ◇ magnitude of velocity vector is $\dot{r} = \|\dot{\mathbf{r}}\| = \sqrt{\dot{\mathbf{r}} \cdot \dot{\mathbf{r}}}$

Normal component of velocity

- the subscript n means **normal** to system boundary
- specifically, \dot{r}_n is
 - ◇ the magnitude
 - ◇ of the component of the velocity vector
 - ◇ along the normal vector to the boundary



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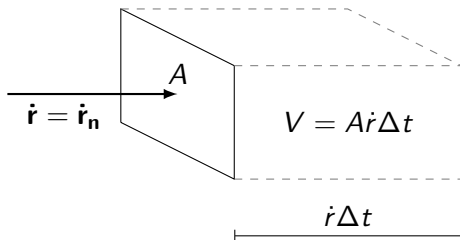
Conservation of mass

Example

One-dimensional flow

- in the one-dimensional flow model,
 - ◇ mass flows are always normal to boundary (so $\dot{\mathbf{r}}_{\mathbf{n}} = \dot{\mathbf{r}}$)
 - ◇ intensive properties are uniform over entrance/exit surfaces
 - ↗ this includes density and velocity of mass flow ↖

Calculating one-dimensional mass flows



- consider one-dimensional flow across a surface of area A
- in time Δt , mass $\Delta m = \rho A\dot{r}\Delta t$ crosses surface
- as $\Delta t \rightarrow 0$,

$$\frac{\Delta m}{\Delta t} \rightarrow \dot{m} = \rho A\dot{r}$$

★ don't mix up density ρ (kg/m^3) and pressure p (kPa)

Calculating non-one-dimensional mass flows

- if the one-dimensional assumptions don't hold, then

$$\dot{m} = \iint_B \rho \dot{r}_n dA$$

- B is the system boundary (in general, a 2D surface in 3D)
- dA is a differential surface area element
- ρ and \dot{r}_n may vary along the boundary
- you'll rarely if ever need this form; if you do, see the textbook

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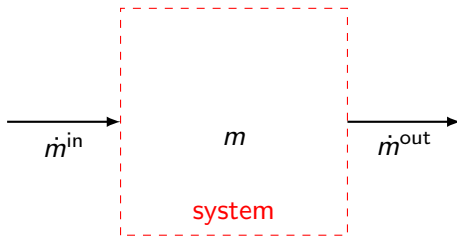
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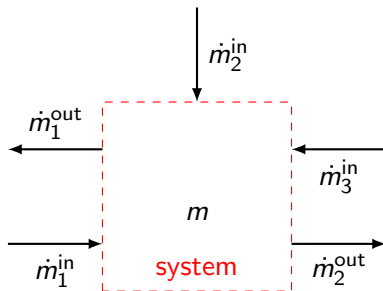
Example

Single-input, single-output form



$$\frac{dm}{dt} = \dot{m}^{\text{in}} - \dot{m}^{\text{out}}$$

Multiple-input, multiple-output form



$$\frac{dm}{dt} = \sum_{i=1}^{N_{\text{in}}} \dot{m}_i^{\text{in}} - \sum_{j=1}^{N_{\text{out}}} \dot{m}_j^{\text{out}}$$

Steady-state form

- in steady state, all properties are constant with respect to time
- in particular, mass (a property) is constant, so $dm/dt = 0$ and

$$\sum_{i=1}^{N_{\text{in}}} \dot{m}_i^{\text{in}} = \sum_{j=1}^{N_{\text{out}}} \dot{m}_j^{\text{out}}$$

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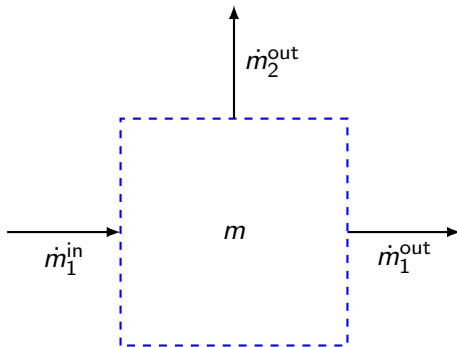
Example

Problem statement

Lake Mead, the reservoir above the Hoover Dam on the Colorado River, initially contains 35 billion m^3 of water. Lake Mead receives 10 billion m^3 per year from the Glen Canyon Dam and other tributaries. The Hoover Dam releases water at an average speed of 0.5 m/s through a cross-sectional area of 700 m^2 . Lake Mead loses 500 million m^3 per year via evaporation. How long until Lake Mead runs dry?



System diagram



Given and find

- **given:**

- ◇ initial volume: $V(0) = 35$ billion m^3
- ◇ final volume: $V(t) = 0$ m^3
- ◇ $\dot{V}_1^{\text{in}} = 10$ billion m^3 per year = 317.1 m^3/s
- ◇ at output 1, $\dot{r} = 0.5$ m/s and $A = 700$ m^2
- ◇ $\dot{V}_2^{\text{out}} = 500$ million m^3 per year = 15.9 m^3/s

- **find:**

- ◇ time t when water volume reaches $V(t) = 0$ m^3

Assumptions and basic equations

- **assume:**

- ◇ one-dimensional flow at output 1
- ◇ time-invariant flow at all inputs and outputs
- ◇ time-invariant, spatially-uniform water density

- **basic equation:**

$$\frac{dm}{dt} = \sum_{i=1}^{N_{in}} \dot{m}_i^{in} - \sum_{j=1}^{N_{out}} \dot{m}_j^{out}$$

Solution

- from conservation of mass,

$$\frac{dm}{dt} = \dot{m}_1^{\text{in}} - \dot{m}_1^{\text{out}} - \dot{m}_2^{\text{out}}$$

- but $m = \rho V$ and ρ is time-invariant and spatially uniform, so

$$\rho \frac{dV}{dt} = \rho \left(\dot{V}_1^{\text{in}} - \dot{V}_1^{\text{out}} - \dot{V}_2^{\text{out}} \right)$$

or

$$\frac{dV}{dt} = \dot{V}_1^{\text{in}} - \dot{V}_1^{\text{out}} - \dot{V}_2^{\text{out}}$$

Solution (continued)

- flow is one-dimensional, so $\dot{m}_1^{\text{out}} = \rho A \dot{r}$, or equivalently,

$$\dot{V}_1^{\text{out}} = \frac{\dot{m}_1^{\text{out}}}{\rho} = A \dot{r} = (700\text{m}^2)(0.5\text{m/s}) = 350\text{m}^3/\text{s}$$

- so volumetric flow rate is

$$\begin{aligned}\frac{dV}{dt} &= \dot{V}_1^{\text{in}} - \dot{V}_1^{\text{out}} - \dot{V}_2^{\text{out}} \\ &= 317.1\text{m}^3/\text{s} - 350\text{m}^3/\text{s} - 15.9\text{m}^3/\text{s} \\ &= -48.8\text{m}^3/\text{s}\end{aligned}$$

Solution (continued)

- since dV/dt is constant,

$$V(t) = V(0) + \left(\frac{dV}{dt} \right) t$$

- therefore,

$$\begin{aligned} t &= \frac{V(t) - V(0)}{dV/dt} = \frac{0\text{m}^3 - 3.5 \times 10^{10}\text{m}^3}{-48.8\text{m}^3/\text{s}} \\ &= 22.7 \text{ years} \end{aligned}$$

